What is Claimed is:

- 1. A method for preparing polyisoprene emulsion articles comprises the steps of.
 - (a) Preparing an aqueous polyisoprene emulsion;
- 5 (b) Blending water-dispersible vulcanization auxiliaries with said aqueous polyisoprene emulsion to form a blended polyisoprene emulsion;
 - (c) Aging said blended polyisoprene emulsion;
 - (d) Adding setting agent into said blended polyisoprene emulsion; and
- (e) Dip-molding said blended polyisoprene emulsion into polyisoprene latex articles.
 - 2. the method, as recited in claim 1, wherein said polyisoprene emulsion in said step (a) is prepared by a free radical emulsion polymerization from isoprene monometers under a normal pressure.
- 3. the method, as recited in claim 1, wherein said polyisoprene emulsion in said step (a) is prepared by a co-polymerization through mixing monometers selected from a group consisted of styrene, acrylates and organic carboxylic acid with isoprene monometers;
- 4. the method, as recited in claim 3, wherein said acrylate is one or more compounds selected from a group consisting of methyl acrylate (MA), ethyl acrylate (EA), butyl acrylate (BA), iso-octyl acrylate (EHA), methyl methacrylate (MMA), and butyl methacrylate (BMA).
- 5. the method, as recited in claim 3, wherein said organic carboxylic acid is 25 one or more compounds selected from a group consisting of acrylic acid (AA),

methacrylic acid (MAA), maleic acid, fumaric acid, and methylenebutene dicarboxylic acid.

- 7. The method, as recited in claim 2, wherein the step (a) further comprises the steps of:
 - (1) Charging a portion of said monomers together with an initiator and an emulsifier into a reactor to form a mixture;
 - (2) Reacting said mixture for 30~60 min. at a room temperature or under a gentle heating;
- 10 (3) Adding dropwise remaining portion of said monomers and other raw materials into said reactor for 3~6 hours.
 - (4) Reacting said mixture under a nitrogen atmosphere for 12~40 hours.
- 8. The method, as recited in claim 6, wherein the step (a) further comprises the steps of:
 - (1) Charging a portion of said monomers together with an initiator and an emulsifier into a reactor to form a mixture;
 - (2) Reacting said mixture for 30~60 min. at a room temperature or under a gentle heating;
- 20 (3) Adding dropwise remaining portion of said monomers and other raw materials into said reactor for 3~6 hours.
 - (4) Reacting said mixture under a nitrogen atmosphere for 12~40 hours.
- 9. The method, as recited in claim 7, wherein said emulsifier in said step (1) is a combination of an anionic emulsifier and a non-ionic emulsifier, said anionic emulsifier is selected from a group consisting of sodium dodecyl sulfate (SDS), sodium

dodecanesulphonate, and OS emulsifier, and said non-ionic emulsifier is nonylphenol polyethylene glycol oxide.

10. the method, as recited in claim 7, wherein a preferred amount of said emulsifier used in said step (1) is 5-30%(by weight), based on total amounts of said monometers.

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- 11. the method, as recited in claim 8, wherein said emulsifier in said step (1) is a combination of an anionic emulsifier and a non-ionic emulsifier, said anionic emulsifier is selected from a group consisting of sodium dodecyl sulfate (SDS), sodium dodecanesulphonate, and OS emulsifier, and said non-ionic emulsifier is nonylphenol polyethylene glycol oxide.
- 12. the method, as recited in claim 8, wherein a preferred amount of said emulsifier used in said step (1) is 5-30%(by weight), based on total amounts of said monometers.
- 13. The method, as recited in claim 7, wherein said initiator used in said step

 (1) a redox system, wherein an oxidant is selected from a group consisting of a watersoluble persulfate and an oil-soluble peroxide; wherein a reductant is selected from a
 group consisting of sodium bisulfite, iron(II) sulfate; wherein a preferred amount of said
 initiator is 0.3-3%(by weight) based on a total amounts of said monometers.
- 20 14. the method, as recited in claim 7, wherein said step (a) further comprises a step adding a co-reductant, a complexing agent and a precipitating agent to maintain a concentration of a ferrous iron (II) ion for ensuring a steady reaction, wherein said co-reductant includes formaldehyde sulfoxylate (rongalite), said complexing agent is ethylenediamine trtraacetic acid (EDTA), and said precipitating agent is pyrophosphates.
 - 15. the method, as recited in claim 7, wherein said water-dispersible vulcanization auxiliaries in said step (b) is selected from a group consisting of

vulcanizators, vulcanization accelerators, age inhibitors, and the like; wherein said vulcanizator is sulfur; said vulcanization accelerator includes sulfenamides and thiurams with an amounts of 0.5~10% (by weight); wherein a preferred amount of said vulcanization accelerator is 1~5% (by weight), based on an amount of said polyisoprene emulsion.

- 16. the method, as recited in claim 8, wherein said water-dispersible vulcanization auxiliaries in said step (b) is selected from a group consisting of vulcanizators, vulcanization accelerators, age inhibitors, and the like; wherein said vulcanizator is sulfur; said vulcanization accelerator includes sulfenamides and thiurams with an amounts of 0.5~10% (by weight); wherein a preferred amount of said vulcanization accelerator is 1~5% (by weight), based on an amount of said polyisoprene emulsion.
- 17. the method, as recited in claim 7, wherein said setting agent used in said step (d) is a mixture of cationic salts and auxiliaries, wherein said cationic salts is selected from a group consisting of hydrochlorides and nitrates of calcium ion, zinc ion, and aluminum ion; wherein a preferred amount of said setting agent is 10-30% (by weight) base on an amount of said polyisoprene emulsion.

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- 18. the method, as recited in claim 8, wherein said setting agent used in said step (d) is a mixture of cationic salts and auxiliaries, wherein said cationic salts is selected from a group consisting of hydrochlorides and nitrates of calcium ion, zinc ion, and aluminum ion; wherein a preferred amount of said setting agent is 10-30% (by weight) base on an amount of said polyisoprene emulsion.
- 19. The method, as recited in claim 7, wherein said step (e) furthering comprises a step for dring said polyisoprene articles at 60~170℃.

- 20. A polyisoprene emulsion, having a weight average molecular weight of weight of 10⁴~10⁵, pH of 6.0-7.0, viscosity of 5-20cp (25°C), solid content of 30-50%, and colloidal size of 100-200nm.
- 21. The polyisoprene emulsion, as recited in claim 20, being made from 60-100 parts by wight of isoprene monometer and 5-50 parts by weight of one or more monometers selected from a group consisting of styrene, acrylates, and organic carboxylic acids.
- 10 22. The polyisoprene emulsion article, as recited in claim 21, containing 10-50% said styrene by weight.
 - 23. The polyisoprene emulsion, as recited in claim 21, containing 10-50% said acrylate by weight.

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- 24. The polyisoprene emulsion, as recited in claim 21, containing 1-10% said organic carboxylic acids by weight.
- 25. A polyisoprene latex article, having a weight average molecular weight of weight of 10⁴~10⁵, pH of 6.0-7.0, viscosity of 5-20cp (25°C), solid content of 30-50%, and colloidal size of 100-200nm.
 - 26. The polyisoprene latex article, as recited in claim 25, being made from 60-100 parts by wight of isoprene monometer and 5-50 parts by weight of one or more monometers selected from a group consisting of styrene, acrylates, and organic carboxylic acids.